

Preparative HPLC Using TSK Columns in the Purification of Biochemical Products

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Preparative HPLC using TSK columns is reviewed. Advantages of preparative HPLC are summarized. Product line is introduced including column dimension and particle size of packing materials. Basic properties of the columns such as performance, calibration curves, mechanical and chemical stability, recovery yields of proteins, titration curves, etc. are described. Sample loading capacity is summarized. An idea for column selection is presented. Typical examples are given. Finally concluded that preparative HPLC will widely be recognized in near future as the best method for the final fine purification step in the commercial production of biopolymers owing to various advantages.

1. Introduction

In the separation of biopolymers, high performance gel filtration chromatography (GFC) has become very popular during the last ten years^{1~21)}. High performance ion exchange chromatography (IEC) has followed GFC during the past three years to be used widely, too^{22~28)}. Now high performance hydrophobic interaction chromatography (HIC) has become available as the third universal liquid chromatographical technique for the separation of biopolymers^{29~31)}.

It goes without saying that these break-throughs have been brought by great advances in the production technology of packing materials having sophisticatedly controlled pore structure and high mechanical strength.

Since HPLC has become widely used in biochemical field as an unparalleledly important method for analysis, the trend to utilize its advantages in the purification of various biochemical substances is also growing rapidly. The direct extension of the best analytical method to the final production plant, if available, can undoubtedly provide various advantages in the total stages from early research to final commercialization.

A typical example for the industrial purification steps of proteins in new biotechnology will be summarized in the comparison with the conventional one as shown in Table 1.

We are engaged in the development of three major techniques, HPLC, MPLC (medium performance liquid chromatography), and UF (ultrafiltration) for new separation technology. HPLC and MPLC will be used widely in place of LPLC (low performance liquid chromatography) for fine purification and rough purification, respectively. UF will play important roles in various steps as shown above.

Now preparative HPLC has reached the level that several hundred grams per day can be

Table 1 Comparison of Separation Techniques in Biotechnology

| | Conventional technique | New technique |
|----------------------------|---|---|
| 1. Liquid/Solid separation | * Ultracentrifugation | * Ultrafiltration |
| 2. Rough purification | * LPLC (IEC) * Salting out * Extraction | * Ultrafiltration * MPLC (IEC, HIC, GFC) |
| 3. Fine purification | * LPLC (IEC, HIC) | * HPLC (IEC, HIC, GFC) |
| 4. Desalting | * LPLC (GFC) | * LPLC (GFC) * Ultrafiltration |
| 5. Concentration | | * Ultrafiltration |

purified full automatically. Practically, preparative HPLC using a large diameter column has come to be used in the commercial production of expensive biochemical substances such as proteins and enzymes.

Here we present a review on preparative HPLC using TSK columns for the purification of biochemical products.

2. Advantages of preparative HPLC

Table 2 lists the advantages of preparative HPLC in large scale commercial production of biochemical substances including R & D stage. Main simple advantages may be high purity of products owing to high resolution and high productivity owing to high speed. The purity of a product is very important, particularly in new biotechnology, to succeed in various time consuming biological tests without the effect of unfavourable contaminants. However, it should be noted that, despite of the image of high price of HPLC, various great cost reducing factors in comparison with LPLC can be pointed out as in Table 2.

Table 2 Advantages of Preparative HPLC in Industrial Purification of Biological Substances

| Advantages in R & D Stage | Fundamental Features | Advantages in Production | |
|---|---|------------------------------|--|
| | | Primary Merits | Cost Reducing Factors |
| * High purity of sample (precise and accurate informations) | * High resolution (sharp peak) | * High purity of product | * Low consumption of raw materials |
| | * High speed | * High recovery | * Low cost in product recovery process |
| | | * High concentration | |
| * Speedy selection & optimization of conditions | * High reproducibility (bed stability) | High productivity | * Low investment |
| | | * Compactness (small column) | |
| * Speedy scale-up | * Availability of high quality prepacked column | * Easiness of automation | * Low labour cost |

Table 3 Typical Example of Large Scale Production by HPLC

| * Separation mode | GFC | IEC |
|--------------------|--------------------|--------------------|
| * Column | TSKgel G3000SW | TSKgel DEAE-5PW |
| * Column size | 108mm I.D. × 600mm | 108mm I.D. × 200mm |
| * Loading capacity | 10g/cycle | 5g/cycle |
| * Cycle/day | 12 | 12 |
| * Cycle/year | 2,400 | 2,400 |
| * Capacity/year | 24,000g | 12,000g |

Particularly, drastic saving of time and money in research and development stage owing to speedy establishment of scale-up is very important not only for cost reduction but also for reaching the goal before any other rivals in severe competition in the development of new bioproducts. Once the conditions are optimized by an analytical column, what a customer has to do for scale-up is only to purchase a corresponding preparative column followed by very slight modifications of the conditions.

In the production, the high recovery yield brought by high resolution and/or speedy operation is a big cost reducing factor affecting the cost of the total process including all preceding steps. In addition, high reproducibility owing to stable column bed leads to easiness of full automation, resulting in drastic reduction of labour cost.

Typical examples of the production capacity in GFC and IEC using a column of 108mm I.D. are given in **Table 3**, which indicates that several tens of kilograms are usually produced per year. The column cost can be estimated less than a few dollars per gram product.

3. TSK columns for preparative HPLC in biochemical field

[1] Kinds of columns

Table 4 lists the main TSK columns for preparative HPLC used for purification of biochemical substances. As shown in **Table 4**, TSK columns cover total field of commonly used separation modes, namely GFC, IEC, HIC and RPC (reversed-phase chromatography). Inner diameters of 21.5, 55.0 and 108 are available for all main columns. Many other columns not listed in **Table 4** such as TSKgel G4000SW, G6000PW, DEAE-3SW, CM-3SW, DEAE-2SW, CM-2SW, SP-2SW, TMS-250 etc. are limited to 21.5mm I.D. size because of inferiority to their alternatives in resolving power or column stability or costwise problem. The column length increase with increasing diameter for IEC and HIC.

Table 5 lists TSK guard columns, essential to preparative HPLC to protect preparative columns.

[2] Particle size

Particle size is increased with increasing column diameter as shown in **Table 6**.

Particle size should be determined to obtain the best compromise among the following factors:

- a) Resolving power: The smaller the particle size, the higher the resolving power¹⁴⁾. However, it should be noted that resolving power can be increased by decreasing flow

rate.

- b) Pressure drop and flow rate: Pressure drop is reversely proportional to the square of particle size. Pressure drop increases with increasing column diameter for the same particle size.
- c) Loading capacity: There is a tendency that maximum loading capacity increases with increasing particle size in the range of small particle size.

Table 4 TSK Columns for Preparative HPLC in Biochemical Field

| Mode | Type | Pore Size (Å) | Column Dimension (mm) | | | Base Material | Typical Sample |
|------|-------------------|---------------|-----------------------|---------|----------|---------------|---|
| | | | 21.5 I.D. | 55 I.D. | 108 I.D. | | |
| GFC | TSKgel G2000SW | 125 | 300,600 | 300,600 | 600 | Silica | Proteins & enzymes |
| | TSKgel G3000SW | 250 | 300,600 | 300,600 | 600 | | |
| | TSKgel G2000PW | 80 | 600 | 600 | 600 | Polymer | Poly- & oligo-saccharides Large proteins |
| | TSKgel G3000PW | 200 | 600 | 600 | 600 | | |
| | TSKgel G5000PW | 1,000 | 600 | 600 | 600 | | |
| IEC | TSKgel DEAE-5PW | 1,000 | 150 | 200 | 200 | Polymer | Proteins & enzymes |
| | TSKgel SP-5PW | 1,000 | 150 | 200 | 200 | | |
| HIC | TSKgel Phenyl-5PW | 1,000 | 150 | 200 | 200 | Polymer | Proteins |
| RPC | TSKgel ODS-120A | 120 | 300 | 300,600 | 300,600 | Silica | Peptides |
| | TSKgel ODS-120T | 120 | 300 | 300,600 | 300,600 | | |

Table 5 TSK Guard Columns for Preparative HPLC

| Mode | Guard Column | Column Dimension (mm) | | |
|------|----------------------------|-----------------------|-----------|------------|
| | | 21.5mm I.D. | 55mm I.D. | 108mm I.D. |
| GFC | TSKguard column SW | 21.5×75 | 45×50 | 83×50 |
| | TSKguard column PW | 21.5×75 | 45×50 | 83×50 |
| IEC | TSKguard column DEAE-5PW | *1 | 45×50 | 83×50 |
| | TSKguard column SP-5PW | | 45×50 | 83×50 |
| HIC | TSKguard column Phenyl-5PW | *1 | 45×50 | 83×50 |
| RPC | TSKguard column ODS-120A | *2 | 45×50 | 83×50 |
| | TSKguard column ODS-120T | | 45×50 | 83×50 |

(Note) *1 Guardgel kits are available.

*2 Bulkgels are available.

Table 6 Relationship between Column Diameter and Particle Size

| Column diameter (mm) | 4.6 | 7.5 | 21.5 | 55 | 108 |
|----------------------|--------------------|-----|------|----|-----|
| | Particle size (μm) | | | | |
| GFC, IEC, HIC | — | 10 | 13 | 20 | 20 |
| RPC | 5 | 10 | 10 | 20 | 20 |

- d) Column life: There is a tendency that column life becomes longer as particle size increases because of lower pressure drop.
- e) Column price: Column price clearly increases with decreasing particle size due to the increases of the sorbent production cost and column packing process cost.

By the adequate particle size selection, TSK preparative HPLC columns, in comparison with the corresponding analytical columns, can provide nearly equal resolving power at a slight expense of speed (see Fig. 19, 26, 30, 31 and 32), reduced pressure drop (see Fig. 4), larger loading capacity (see Fig. 15), longer column life and much reduced price relatively.

[3] Base material

Modern liquid chromatography sorbents consist of three major base materials, namely silica gel, cross-linked polymer gel and cross-linked polysaccharide gel.

Base materials for sorbents for TSK preparative HPLC columns consist of silica gel and cross-linked polymer gel. The advantages of these materials are well utilized complementally each other, namely the high performance of the silica gel in GFC and RPC and the chemical stability of the cross-linked polymer gel in IEC and HIC, respectively.

The silica gel, featured by high mechanical strength and nonswelling and nonshrinking property against solvent exchange, is the main material for HPLC sorbents, particularly RPC. Another big advantage of the silica gel is its excellent pore characteristics in the range of 100 to 500 angstrom such as homogeneous pore distribution and large pore volume, realizing excellent resolution of proteins in GFC.

The cross-linked polymer gel, featured by excellent chemical stability and various well-balanced properties such as semi-rigidity, small swelling and shrinking, availability of variety of pore size etc., is increasingly used as the second material for HPLC sorbent. The chemical stability of sorbents is very important particularly in preparative IEC and HIC in which sorbents usually tend to be deteriorated easily by strong adsorption of various complex substances due to ionic or hydrophobic interaction and should be cleaned up frequently by strong alkaline or acidic solutions.

The cross-linked polysaccharide gel, featured by excellent hydrophilicity, has widely been used for the separation of biopolymers. However, its application to HPLC has been seriously restricted because of the mechanical weakness.

4. Basic properties of TSK preparative HPLC columns

[1] Performance

Table 7 lists the particle size, theoretical plate number, flow rate and pressure drop of the series of the columns.

Most of the theoretical plate numbers guaranteed per column are higher or equal to those of the corresponding analytical columns.

[2] Calibration curves and average pore sizes

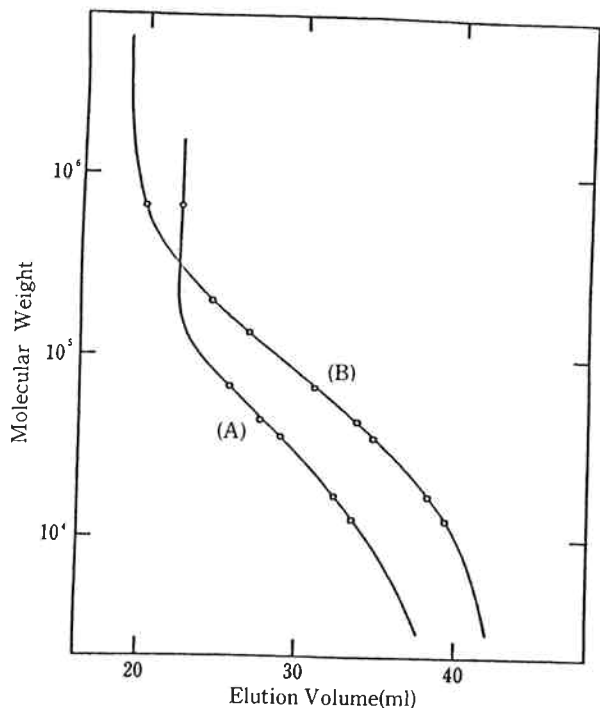
Fig. 1 and 2 show the calibration curves of TSKgel G2000SW and G3000SW for proteins²⁾ and TSKgel G2000PW, G3000PW and G5000PW for polysaccharide and oligosaccharide, respectively²⁾. The former indicates that the SW columns have perfectly fitting pore size and pore distribution for the separation of proteins.

Table 7 Specifications of TSK Columns for Preparative HPLC

| Type | Column Dimension (mm I.D. × mm) | Particle Size (micron) | Theoretical Plates per Column | Flow Rate (ml/min) | | Maximum Pressure (kg/cm ²) |
|------------------------------------|------------------------------------|---------------------------|-------------------------------|-----------------------|---------|---|
| | | | | Suitable | Maximum | |
| TSKgel G2000SW | 21.5 × 300 | 13 | 5,000/EG | 4-6 | 8 | 10 |
| | 21.5 × 600 | 13 | 10,000/EG | 4-6 | 8 | 15 |
| | 55.0 × 600 | 20 | 700/BSA | 15-25 | 50 | 15 |
| | 108.0 × 600 | 20 | 700/BSA | 50-100 | 150 | 15 |
| TSKgel G3000SW | 21.5 × 300 | 13 | 5,000/EG | 4-6 | 8 | 15 |
| | 21.5 × 600 | 13 | 10,000/EG | 4-6 | 8 | 20 |
| | 55.0 × 600 | 20 | 1,800/BSA | 15-25 | 50 | 15 |
| | 108.0 × 600 | 20 | 1,800/BSA | 50-100 | 150 | 15 |
| TSKgel G2000PW | 21.5 × 600 | 17 | 10,000/EG | 4-6 | 8 | 10 |
| | 55.0 × 600 | | | | | |
| | 108.0 × 600 | | | | | |
| TSKgel G3000PW | 21.5 × 600 | 17 | 10,000/EG | 4-6 | 8 | 15 |
| | 55.0 × 600 | | | | | |
| | 108.0 × 600 | | | | | |
| TSKgel G5000PW | 21.5 × 600 | 22 | 6,000/EG | 4-6 | 8 | 5 |
| | 55.0 × 600 | | | | | |
| | 108.0 × 600 | | | | | |
| TSKgel DEAE-5PW | 21.5 × 150 | 13 | 3,000/C5'M | 4-6 | 8 | 2 |
| | 55.0 × 200 | 20 | 1,500/C5'M | 20-30 | 50 | |
| | 108.0 × 200 | 20 | | | | |
| TSKgel SP-5PW | 21.5 × 150 | 13 | 3,000/Cyt | 4-6 | 8 | 10 |
| | 55.0 × 200 | 20 | 1,500/Cyt | 20-30 | 50 | 3 |
| | 108.0 × 200 | 20 | | | | |
| TSKgel Phenyl-5PW | 21.5 × 150 | 13 | 2,000/Acet | 4-6 | 8 | 3 |
| | 55.0 × 200 | 20 | 1,500/Acet | 20-30 | 50 | |
| | 108.0 × 200 | 20 | | | | |
| TSKgel ODS-120A TSKgel ODS-120T | 21.5 × 150 | 10 | 8,000/Bz(T) /Ph(A) | 4-6 | 10 | 20 |
| | 55.0 × 300 | 20 | 3,000/Bz(T) | 30-60 | 100 | |
| | 55.0 × 600 | 20 | 6,000/Bz(T) | 15-40 | 50 | |
| | 108.0 × 300 | | | | | |
| | 108.0 × 600 | | | | | |

(Note) Samples for measurement of theoretical plates number :

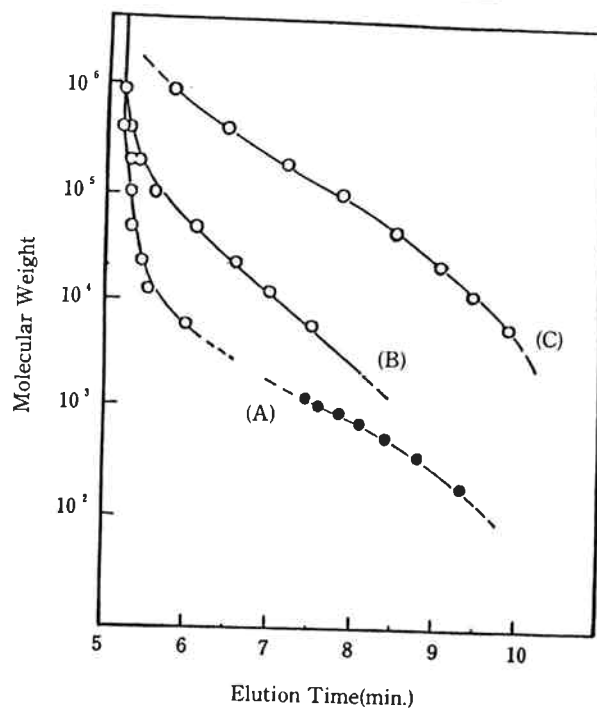
- EG ; ethylene glycol
- BSA ; bovine serum albumin
- C5'M ; cytidine 5' monophosphate
- Cyt ; cytidine
- Acet ; acetone
- Bz ; benzene
- Ph ; phenol



Column : (A) TSKgel G2000SW
 (B) TSKgel G3000SW
 Sample : Protein
 Eluent : 0.2M Phosphate buffer (pH 6.8)
 Flow rate : 1.0ml/min.
 Detector : UV 280nm

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Fig. 1 Calibration Curves of TSKgel G2000SW and G3000SW for Protein



Column : (A) TSKgel G2000PW
 (B) TSKgel G3000PW
 (C) TSKgel G5000PW
 Sample : (○) Pullulan Standards
 (●) Hydrolyzed β -Cyclodextrin
 Eluent : Distilled water
 Flow rate : 1.0ml/min
 Detector : RI

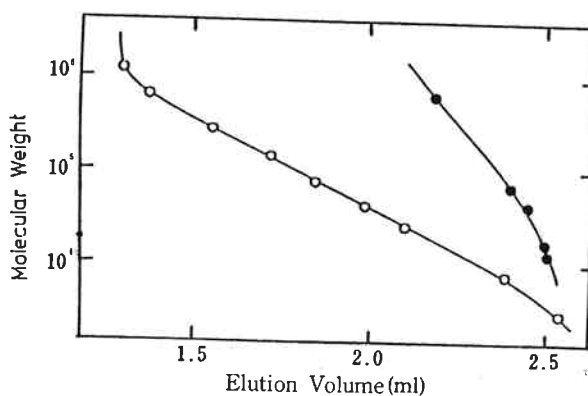
Fig. 2 Calibration Curves of TSKgel G2000PW, G3000PW and G5000PW for Pullulan

Fig. 3 shows the calibration curve of TSKgel DEAE-5PW for proteins and poly (ethylene oxide)²⁴, indicating that the pore size is so large that even large proteins like thyroglobulin can easily penetrate into the pore. Other G5000PW gel based columns such as TSKgel SP-5PW and Phenyl-5PW have the same calibration curves.

Average pore sizes are listed in Table 4. TSKgel ODS-120A & T have so large pore size as universal ODS columns to cover even small proteins.

[3] Mechanical stability of TSK preparative HPLC columns

Figs. 4 to 7 show the flow rate dependence of pressure drop on TSKgel SW, PW, DEAE-5PW, SP-5PW, Phenyl-5PW, and ODS-120T



Column : TSKgel DEAE-5PW,
 7.5mm I.D. \times 75mm
 Sample : (●) Proteins
 (○) Polyethylene glycols
 Eluent : 0.1M Phosphate buffer (pH 5.5) + 0.5M NaCl and Distilled water
 Flow rate : 1.0ml/min.
 Detector : RI and UV 280nm

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Fig. 3 Plots of Molecular Weights against Elution Volumes for Proteins and Polyethylene Glycols on TSKgel DEAE-5PW

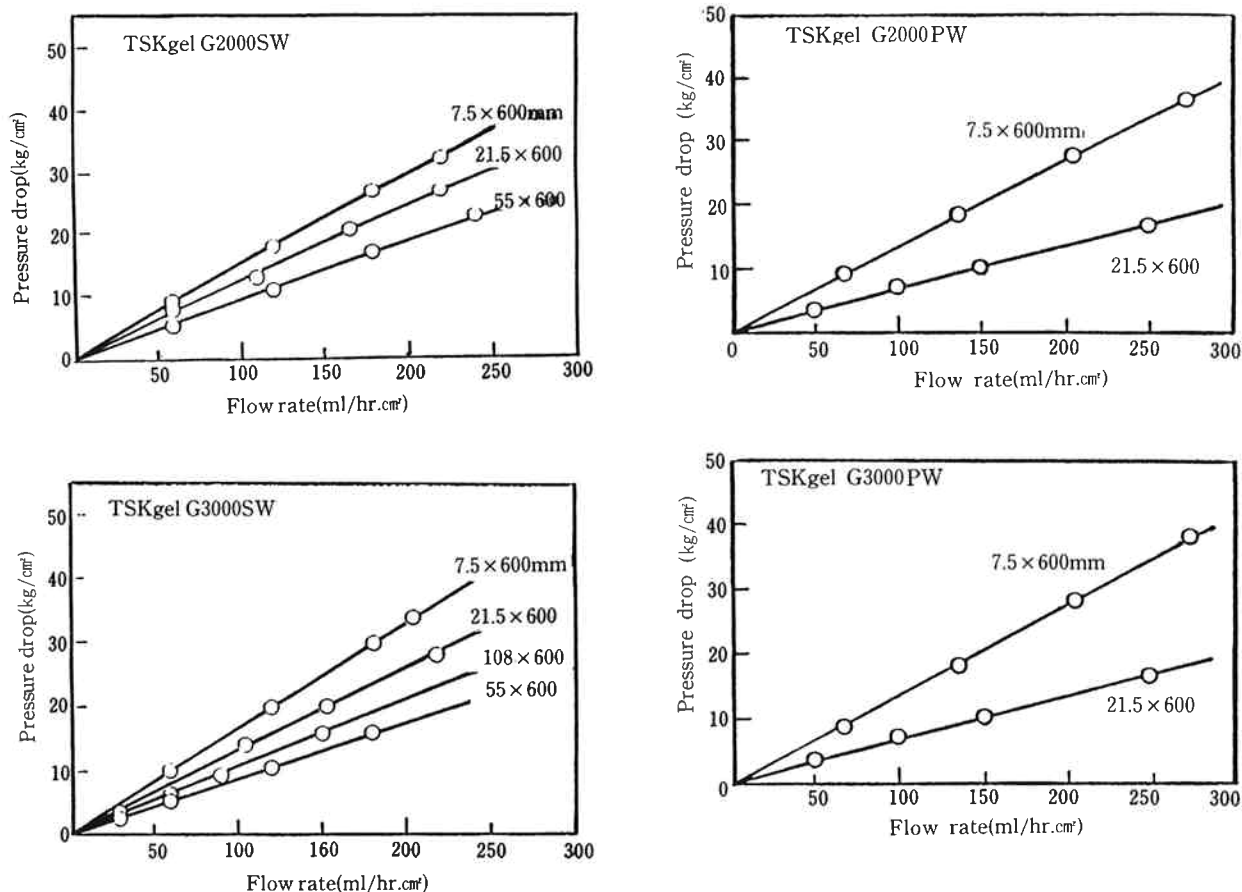


Fig. 4 Flow Rate Dependence of Pressure Drop on TSKgel G2000SW and G3000SW Columns.

columns, respectively. Excellent linearity indicates the mechanical stability of these columns.

[4] Chemical stability of sorbents

Table 8 shows the stability of TSKgel DEAE-5PW, SP-5PW and Phenyl-5PW against strong alkaline and acidic solutions. Ionic capacities or the amount of phenyl group of these sorbents were checked before and after the exposure to the solution and no change was observed.

[5] Recovery of proteins and their activity

The loss of recovery is mainly caused by the following three factors:

- Adsorption to the sorbent: to avoid this factor TSKgels are designed to be sufficiently hydrophilic with inert hydroxyl groups and ether bonding.
- Spontaneous denaturation during the purification process: high speed operation of HPLC is very effective to improve the recovery yield of the activity of labile biopolymers.
- Peak overlapping: the HPLC method is obviously the best to obtain the highest yield

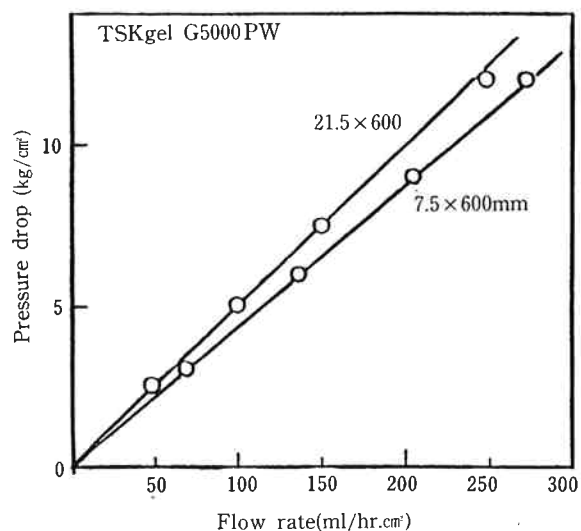


Fig. 5 Flow Rate Dependence of Pressure Drop on TSKgel G2000PW, G3000PW and G5000PW Columns.

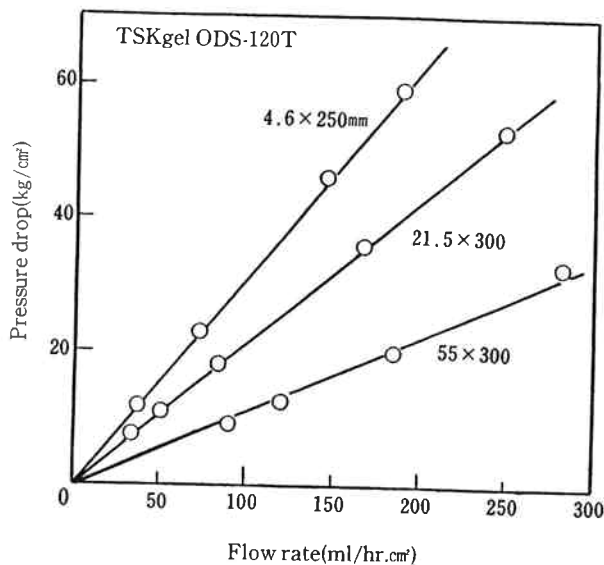
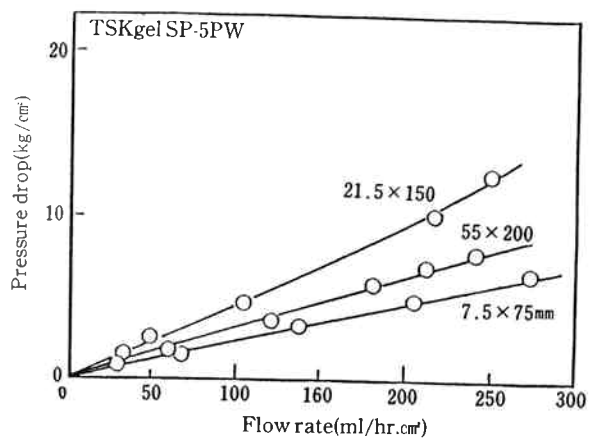
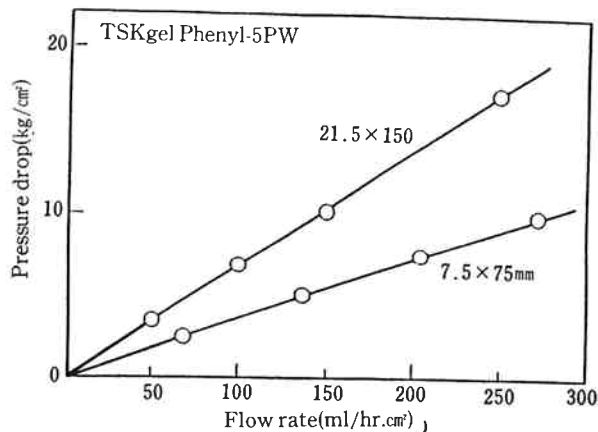
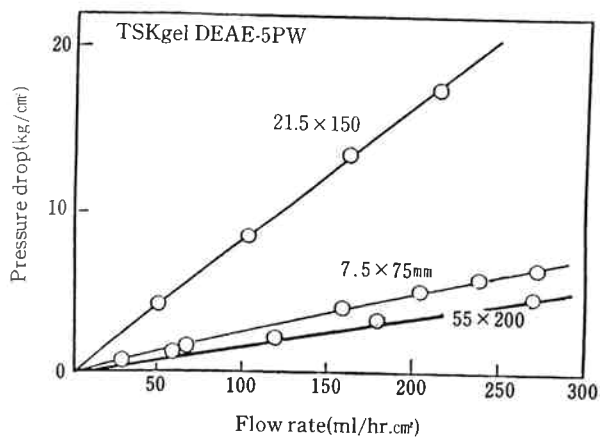


Fig. 6 Flow Rate Dependence of Pressure Drop on TSKgel DEAE-5PW and SP-5PW Columns.

Fig. 7 Flow Rate Dependence of Pressure Drop on TSKgel Phenyl-5PW and ODS-120T Columns.

Table 8 Stability of TSKgel DEAE-5PW, SP-5PW and Phenyl-5PW Against Strong Alkaline and Acidic Solution

| Ion-exchanger | Solution | Ion-exchange capacity (meq/ml) | |
|---------------|--------------------------|--------------------------------|----------------|
| | | Before exposure | After exposure |
| DEAE-5PW | 0.5 N NaOH | 0.09 | 0.09 |
| DEAE-5PW | 0.5 N HCl | 0.09 | 0.09 |
| DEAE-5PW | 20% CH ₃ COOH | 0.09 | 0.08 |
| SP-5PW | 0.5 N NaOH | 0.13 | 0.13 |
| SP-5PW | 0.5 N HCl | 0.13 | 0.13 |
| SP-5PW | 20% CH ₃ COOH | 0.13 | 0.13 |
| | | Phenyl group content (mmol/ml) | |
| | | Before exposure | After exposure |
| Phenyl-5PW | 0.5 N NaOH | 0.105 | 0.104 |
| Phenyl-5PW | 20% CH ₃ COOH | 0.105 | 0.106 |

Samples were exposed in alkaline or acid solution for 10 days at 25°C

Table 9 Recovery of Proteins from TSKgel G3000SW

| | pH=6.9 | | | pH=7.8 |
|------------------------------|---|---|------------------------|------------------------------|
| | 0.2M KH_2PO_4 +0.2M K_2HPO_4 | 0.2M NaH_2PO_4 +0.2M Na_2HPO_4 | 0.05M PB +0.2M NaCl | 0.05M Tris-HCl +0.2M NaCl |
| Lysozyme | 96% | 92% | 94% | 75% |
| Cytochrome C | 101 | 98 | 98 | 92 |
| α -Chymotrypsinogen A | 98 | 95 | 92 | 90 |
| γ -Globulin | 98 | 95 | 98 | 88 |
| Thyroglobulin | 94 | 94 | 87 | 85 |
| Ovalbumin | 92 | 96 | 68 | 66 |

Elution condition

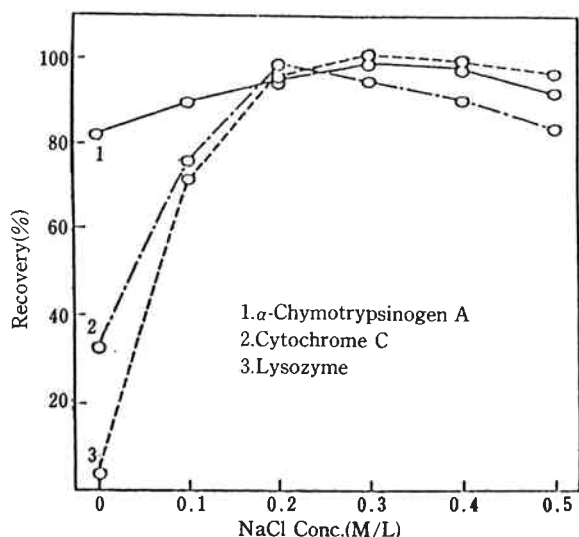
Column : TSKgel G3000SW, 7.5mm I.D. \times 600mm

Load : Concentration 0.3–0.5%

Injection volume 200 μ l

Flow rate: 1.0ml/min.

Detector : UV 280nm



Column : TSKgel G3000SW

Eluent : 0.05M Phosphate buffer (pH6.9) + NaCl

Load : 60 μ g

Fig. 8 Effect of Salt Concentration on Recovery

by avoiding peak overlapping owing to the high resolution.

The following data shows that unfavourable adsorption of these proteins is not observed on TSK columns.

Table 9 shows the recovery yields of proteins on TSKgel G3000SW column with several typical eluents¹⁴⁾. Fig. 8 shows the effect of salt concentration on the recovery yield of basic proteins on TSKgel G3000SW column¹⁴⁾.

Table 10 shows the recovery yields of

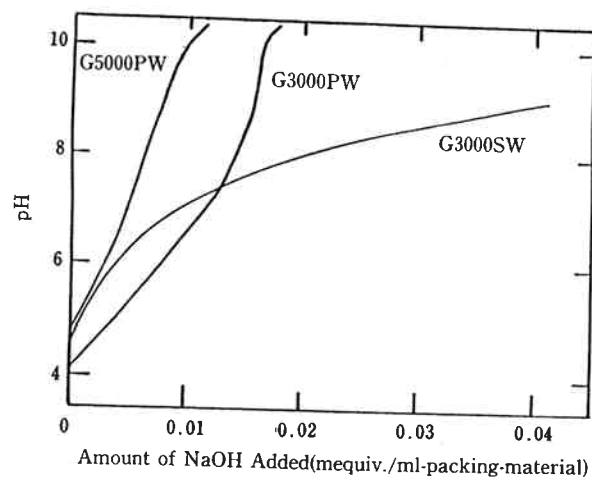
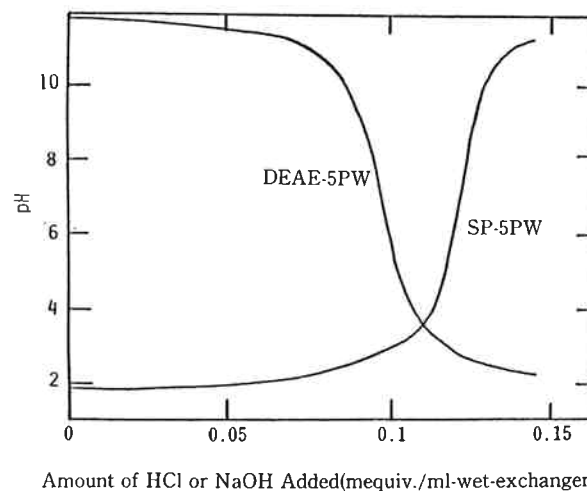


Fig. 9 Titration Curve of TSKgel G3000PW, G5000PW and G3000SW



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Fig. 10 Titration Curve of TSKgel DEAE-5PW and SP-5PW

Table 10 Recovery of Proteins from TSKgel DEAE-5PW, SP-5PW and Phenyl-5PW

DEAE-5PW

| Protein | Recovery (%) |
|------------------------|--------------|
| Thyroglobulin | 98 |
| Ferritin | 99 |
| γ -Globulin | 100 |
| Bovine serum albumin | 102 |
| Hemoglobin | 96 |
| Ovalbumin | 104 |
| β -Lactoglobulin | 103 |
| Trypsin inhibitor | 104 |
| Myoglobin | 103 |

Each protein of 0.4mg was applied to DEAE-5PW column (75 \times 7.5mm I.D.) in 0.02 M tris-HCl buffer (pH 8.5) and the adsorbed protein was desorbed in 0.02M tris-HCl buffer (pH 8.5) containing 0.5M NaCl.

SP-5PW

| Protein | Recovery (%) |
|------------------------------|--------------|
| γ -Globulin | 98 |
| Hemoglobin | 96 |
| Trypsinogen | 101 |
| α -Chymotrypsinogen A | 98 |
| α -Chymotrypsin | 104 |
| Myoglobin | 88 |
| Lysozyme | 95 |
| Ribonuclease A | 100 |
| Cytochrome C | 103 |

Each protein of 0.4mg was applied to SP-5PW column (75 \times 7.5mm I.D.) in 0.02 M phosphate buffer (pH 6.0) and the adsorbed protein was desorbed in 0.02 M phosphate buffer (pH 6.0) containing 0.5M NaCl.

Phenyl-5PW

| Protein | Recovery (%) |
|----------------------------|--------------|
| Bovine serum albumin | 102 |
| Ovalbumin | 111 |
| α -Chymotrypsinogen | 99 |
| α -Chymotrypsin | 109 |
| Myoglobin | 101 |
| Lysozyme | 92 |
| Ribonuclease | 104 |
| Cytochrome C | 106 |

Proteins were adsorbed in 0.1M phosphate buffer containing 2 M ammonium sulfate (pH 7.0) and desorbed in 0.1M phosphate buffer (pH 7.0) at 25°C.

Proteins of 0.5 mg each were applied to the column of 75 \times 7.5mm I.D.

Recovery of Enzymatic Activity from TSKgel DEAE-5PW

| Enzyme | Recovery (%) |
|------------------------|--------------|
| Catalase | 80 |
| Lipoxidase | 95 |
| α -Chymotrypsin | 93 |

Recovery of Enzymatic Activity from TSKgel SP-5PW

| Enzyme | Recovery (%) |
|------------------------|--------------|
| Lipoxidase | 84 |
| α -Chymotrypsin | 97 |
| β -Amylase | 88 |

Recovery of Enzymatic Activity from TSKgel Phenyl-5PW

| Enzyme | Recovery (%) |
|-----------------------------------|--------------|
| α -Chymotrypsin (0.4mg) | 92 |
| Lipoxidase (1.0mg) | 89 |
| Ferredoxin NADP reductase (3.0mg) | 100 |
| β -Amylase (1.3mg) | 80 |
| Lysozyme (0.2mg) | 90 |
| Lysozyme (0.05mg) | 90 |

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